





Optimal HVAC control for state-of-the-art office building: methodology and open questions


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Model predictive control

$\min J(x, u)$  Cost

s.t. $\dot{x} = f(x, u)$  System

$0 = h(x, u)$ 

$0 \leq g(x, u)$ 

Constraints

System



System

- Building envelope
 - Zones
 - Glazing
 - Walls
- Occupants and internal gains
- Controls

System

- HVAC

- Ventilation

- Heat exchangers
- Fans
- Ducts
- Chiller
- VAV
- Humidifier



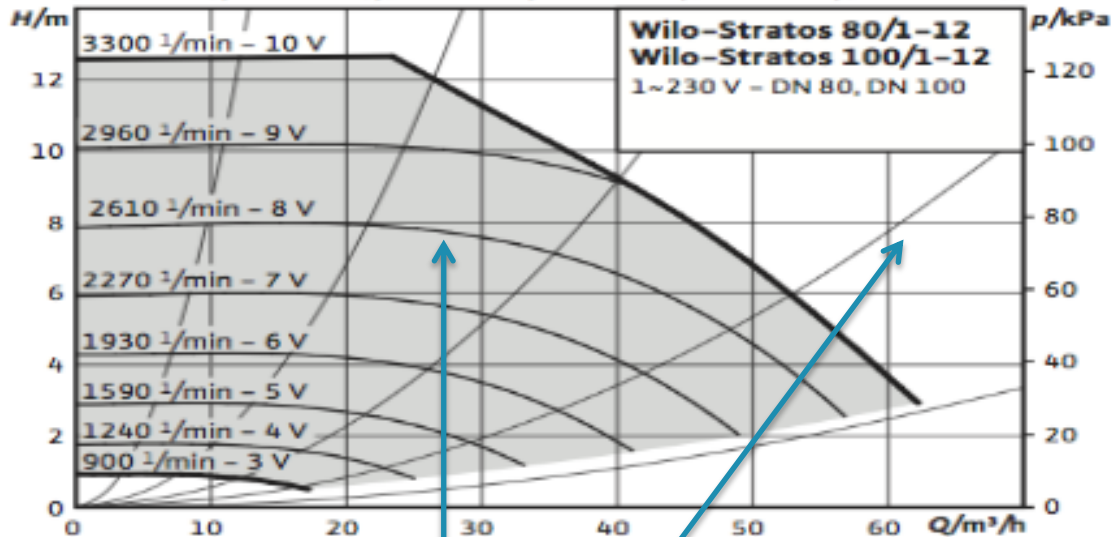
- HVAC

- Hydronics

- Heat exchangers
- Pump
- Pipes
- Heat pump
- Valve
- Heater
- Solar collector
- Thermal storage
- Bore field
- Concrete core activation

System (non-)linearities

- Building envelope: I
 - Thermal conducti
 - Thermal convecti
 - Thermal radiator
- Heat exchangers: r
 - NTU method:
- Speed controlled fans/pumps:
 - Similarity laws
 - Pump curve
 - Load curve



$$\frac{\dot{m}_1}{\dot{m}_2} = \frac{n_1}{n_2}$$

$$\dot{m}_1 = f(dp_1)$$

$$\frac{dp_1}{dp_2} = \left(\frac{n_1}{n_2}\right)^2$$

$$\dot{m}_2 = f(dp_2)$$

$$\frac{P_1}{P_2} = \left(\frac{n_1}{n_2}\right)^3$$

System (non-)linearities

- Ducts / pipes
 - Load curve for fan / pump!
 - Conservation of mass
 - Perfect mixing of energy: $\frac{dT}{dt} = -\frac{(T - T_{in})\dot{m}}{m_{pipe}}$
 - Discontinuous mixing in splitter around zero flow
- Chiller / heat pump, heater similar

$$Q = f(T_1, T_2, \dots)$$

$$COP = f(T_1, T_2, \dots)$$

$$Pel = \frac{Q}{COP}$$

$$T_{out} = T_{in} + \frac{Q}{\dot{m}c_p}$$

System (non-)linearities

- Thermal storage
 - Bi-directional flows
 - Mixing or stratified temperature?

$$m_{tot} = m_{hot} + m_{cold}$$

$$E_{hot} = c_p \cdot T_{hot} \cdot m_{hot}$$

$$\frac{dE_{hot}}{c_p dt} = \dot{m}_{in} \cdot T_{in} - \dot{m}_{out} \cdot T_{hot}$$

- Internal/external gains: non-linear functions of time

System dynamics

- Fast dynamics:
 - Sensors
 - Pipes
 - Air temperature
 - Heat production devices
- Slow dynamics
 - Building envelope

Approach for MPC

- Fast dynamics -> small time steps -> slow
 - Neglect fast dynamics
- Building envelope
 - Large state space
 - -> Model order reduction
 - *But which techniques to use?*
 - Asymptotic waveform evaluation
 - Arnoldi method
 - Laguerre method
 - Truncation method
 - Hankel norm reduction
 - Proper orthogonal decomposition, etc

Approach for MPC

- Simplify pipe hydraulics: $Q = \dot{m}c_p\Delta T$
 - Into:
 - Q
 - $Q < \dot{m}_{nom} \cdot c_p \cdot \Delta T$
 - $Q < \Delta T_{nom} \cdot c_p \cdot \dot{m}$
- Heat exchanger
 - $Q < a \cdot (T_1 - T_2) = Q_{max}$
 - Post-processing using mass flow rate required
 - *Problem if bi-directional heat flow or fixed mass flow rate*
 - *How to obtain feasible solution?*

Approach for MPC

- Pumps/fans
 - Ignore pressure drops, control mass flow rate directly
 - Fit cost curve based on expected working points:

$$P_{el,pump} = c_1 + c_2 \cdot \dot{m} + c_3 \cdot \dot{m}^2$$

$$\dot{m} \leq \dot{m}_{max}$$

- Post-processing required for finding pump speed
- *Sub-optimal -> better approach?*

Approach for MPC

- Heat pump

Q

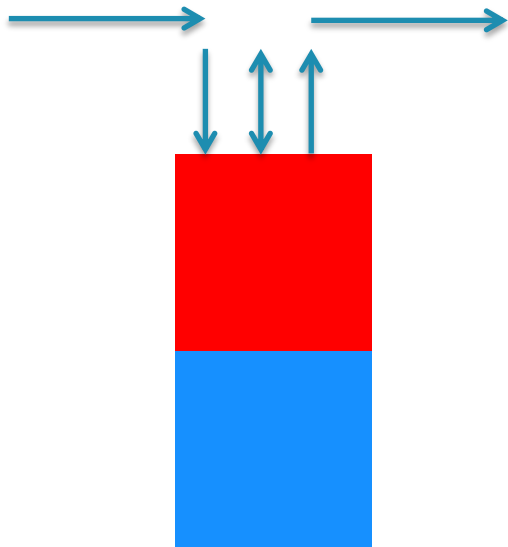
$$Q < Q_{max} = f(T)$$

$$P_{el} = \frac{Q}{COP_{nom}} \neq f(T) \dots$$

- *Time modulation for Q?*

Approach for MPC

- Thermal storage



$$m_{tot} = m_{hot} + m_{cold}$$

$$E_{hot} = c_p \cdot T_{hot} \cdot m_{hot}$$

$$\frac{dE_{hot}}{c_p dt} = \dot{m}_{in} \cdot T_{in} - \dot{m}_{out} \cdot T_{hot}$$

- *Calculation using Q? But then no way to find T*
- *Force $T = T_{high}$ to be constant, but then suboptimal*
- Internal gains: inputs

Conclusion

- Building: linear
 - Model order reduction, but which technique to use?
- HVAC:
 - Can use heat flows Q -> linear
 - But how to reformulate constraints and cost function?
 - Generic way for performing post-processing?

