## Exercises 14: Course revision and exam preparation (Thursday 11.02.2016 at 15:00 in Room SR 00 014)

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1. Consider a process plant that is described by the nominal transfer function

$$\hat{G}(s) = \frac{(3-s)}{(s+1)(s+5)}$$

with a multiplicative model uncertainty that has as an upper bound

$$\bar{\Delta}_{\mathrm{M}}(s) = 0.1 \cdot \frac{s+1}{\frac{s}{100}+1}$$
.

We want to design a robust and stable discrete-time controller  $K_z(z)$  with internal model control (IMC). The goal is to achieve the maximal possible bandwidth for the closed-loop system, while still guaranteeing robust stability. The controller design is done in the continuous-time domain. Afterwards the controller is digitized.

- (a) Is the nominal plant model  $\hat{G}(s)$  minimum-phase?
- (b) Determine the ideal IMC-controller  $K^*_{\text{IMC}}(s)$  that minimizes the integral square error (ISE) for step reference inputs. Factorize  $\hat{G}(s)$  if necessary.
- (c) We now add a filter  $V_{\rm f}(s) = \frac{1}{(Ts+1)^n}$  in order to make the controller  $K_{\rm IMC}(s)$  proper. Choose a filter of the lowest possible order to achieve this. Determine a lower limit for the filter time constant T, by taking into consideration the condition for robust stability.

*Hint:* Draw the Bode-diagram of the robustness limit, computed with the upper bound of the multiplicative uncertainty  $\bar{\Delta}_{M}(s)$ .

- (d) Determine the transfer function of the overall controller K(s).
- (e) Determine the discrete equivalent  $K_z(z)$  of the overall controller K(s) designed above. Use the zero-pole matching method. Use the sampling period  $T_p = 25$ ms
- 2. Consider a process plant described by the transfer function

$$G(s) = \frac{e^{-T_{\rm d}s}}{(5s+1)(2s+1)} \,.$$

Design a Smith Predictor that realizes a feedback loop with a settling time  $T_s \leq T_d + 3 \text{ sec}$ , and with an overshoot  $M_p \leq 10\%$ . The dead time  $T_d = 42 \text{ sec}$ .

- (a) Design a lead compensator  $K_{\rm R}(s) = k_{\rm D} \frac{T_{\rm D}s+1}{T'_{\rm D}s+1}$  for the rational part  $G_{\rm R}(s)$  of the process plant, using the root locus method.
  - i. What are the desired pole locations of the closed-loop system poles?
  - ii. Determine the lead zero  $\frac{1}{T_{\rm D}}$  in order to cancel the slowest process pole.
  - iii. Determine the lead pole  $\frac{1}{T'_{D}}$  in order to fix the real part of the closed-loop poles.
  - iv. Determine the gain  $k_{\rm D}$  in order to place the closed-loop poles in their desired locations.
- (b) Compute the resulting closed-loop transfer function  $G_{\rm r}(s)$ . Assume that the model of the plant is perfect.
- (c) What is the steady state error of the closed-loop system for a step input? And for a ramp input?
- (d) Design a prefilter feedforward controller  $K_{\rm ff,p}(s)$  for a servo application, that minimizes the ISE for step reference inputs. The prefilter should reduce the steady state error for a ramp input to  $e_{\rm ss} \leq 0.1$ . Check if the dynamic requirements are still met.
- 3. A process plant G(s) can be divided into two partial processes  $G_1(s)$  and  $G_2(s)$  in series. The transfer functions of these partial processes are given by

$$G_1(s) = \frac{3}{(2s+1)(4s+1)}$$
 and  $G_2(s) = \frac{4}{15s+1}$ .

Design a cascaded controller that realizes a closed-loop system with a bandwidth  $\omega_{BW,cl} \approx 0.04 \frac{rad}{s}$ .

(a) Design a causal controller  $K_1(s)$  with internal model control (IMC) for the inner loop process  $G_1(s)$ . Minimize the Integral Square Error (ISE). Make sure that the inner loop bandwidth is approximately  $\omega_{BW,1} \approx 0.25 \frac{rad}{s}$ .

- (b) Approximate the obtained inner closed-loop system by a first order system  $G_a(s) = \frac{k_a}{T_a s + 1}$ .
- (c) Design a realizable controller  $K_2(s)$  with internal model control (and with minimal ISE) for the overall process  $G_a(s)G_2(s)$ . Make sure that the bandwidth requirement is met.
- (d) Evaluate the validity of the approximation of the inner closed-loop system, computed in 3b.
- 4. Consider the following system, of which the state space model is decomposed into Kalman form:

$$\dot{\mathbf{x}}(t) = \begin{bmatrix} 2 & -3 & 0 \\ 0 & -1 & 0 \\ 2.8 & 0 & -2 \end{bmatrix} \mathbf{x}(t) + \begin{bmatrix} \sqrt{2} \\ 0 \\ -2 \end{bmatrix} u(t)$$
$$y(t) = \begin{bmatrix} \frac{1}{\sqrt{2}} & \frac{1}{\sqrt{2}} & 0 \end{bmatrix} \mathbf{x}(t) .$$

- (a) Evaluate the controllability and observability of the different states.
- (b) Is the system controllable? If not, is it stabilizable? Is the system observable? (If not, is it detectable?)
- (c) Compute the transfer function of this system. Also, determine that state space model that is a minimal realization of this transfer function.
- (d) Given the state space model obtained in 4c, determine the desired pole locations  $\lambda_{cl,i}$ , so that the closed-loop system has a settling time  $T_s \leq 0.3$  sec.
- (e) If the system is *at least* stabilizable and detectable, determine by 'comparison of coefficients' the feedback controller matrix K that places the closed-loop poles at the desired locations  $\lambda_{cl,i}$ .

Peak time $T_{\rm m}$ $-\frac{\pi}{\sqrt{\pi}}$	$\phi_{\zeta}$	ζ	$\Delta h$	
	$\omega_0 \sqrt{1-\zeta^2}$	66°	0.4	25%
Rise time $T_{\rm r}$	$\frac{1.8}{\omega_0}$	54°	0.58	10%
Settling time $T_{5\%}$	$\frac{3}{\zeta\omega_0}$	45°	0.7	5%
Settling time $T_{2\%}$	$\frac{4.5}{\zeta \omega_0}$	37°		2%
·		36	0.8	270

Table 1: Dynamic behaviour heuristics of a second order system with complex conjugate poles  $\zeta \omega_0 \pm j \omega_0 \sqrt{1-\zeta^2}$ .

Rise time $T_{\rm r}$	$\frac{2.2}{ s_1 }$
Settling time $T_{5\%}$	$\frac{3}{ s_1 }$

Table 2: Dynamic behaviour heuristics of a first order system.

Rise time $T_{\rm r}$	$\frac{3.36}{ s_{1/2} }$	
Settling time $T_{5\%}$	$\frac{4.8}{ s_{1/2} }$	

Table 3: Dynamic behaviour heuristics of a second order system with a double negative real pole.